



## Analysis of Fingering Phenomena in Fractured Porous Media Considering Interface Saturation Variation and Capillary Pressure Effects

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### Abstract

This paper studies fingering phenomena in fractured porous media. A non-linear equation for water saturation is derived and simplified using similarity transformation. The solution is obtained using a power series method. Convergence is discussed using boundedness assumptions, and an approximate solution is obtained by truncating the series. Results show that saturation increases with time and distance, which agrees with physical behavior with the effect for some interesting choices of parametric data value and appropriate boundary condition and graphical and numerical presentation.

**Keywords:** Fingering Phenomenon, Capillary pressure, Similarity Transformation, Fractured Porous Media, Power Series Method

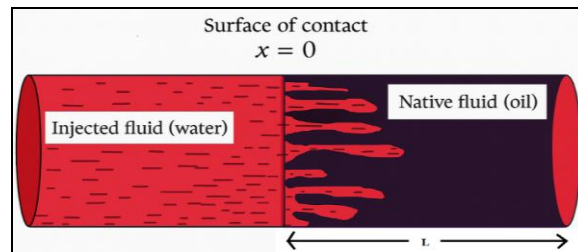
### Introduction

An oil reservoir consists of a porous material, with its pores filled with various hydrocarbon substances, commonly referred to simply as "oil." The heterogeneous nature of the porous medium indicates that properties of the rock, such as porosity and permeability, can differ significantly across various locations. The oil fields known as "fractured oil fields" are the most diverse, comprising clusters of porous medium blocks that are divided by a network of fractures. In the initial recovery stage, oil is drawn from the reservoir without any outside help. The subsequent recovery stage involves the retrieval of leftover oil that is held in the porous structure by introducing different fluids like water, gas, steam, or polymers. Issues, such as fingering, occur because of the pressure from the injected fluids, while differences in viscosity and wetting properties between oil and water lead to the development of these issues at their boundary. The injected water moves swiftly through the porous material along networked capillaries that resemble fingers; thus, this occurrence is known as the fingering phenomenon. Many researchers have discussed this phenomenon in homogeneous and heterogeneous porous medium from various point of view. Vyas N. B *et al.* <sup>[14]</sup> have discussed the magnetic field effect on saturation of injected water with or without magnetic field effect by applied the power series method. Mistry P.R *et al.* <sup>[8]</sup> have presented mathematical model by use of mass flow rates of oil water in equation of continuity and no linear differential equation for obtained saturation of injected water. Patel S.S <sup>[17, 18]</sup> Studied in viscous fingering with perturbation Technique. Borana *et al.* <sup>[4]</sup> applied the Crank-Nicolson finite difference scheme for solution of saturation of water in homogeneous porous medium. Scheidegger <sup>[19]</sup> has provided an overview of the instabilities associated with displacement fronts in porous materials and highlighted the most relevant technique for oil extraction in the field of reservoir engineering, it is important to keep the fingers steady. Verma <sup>[2]</sup> examined the statistical characteristics of fingering that happen during a displacement process in a heterogeneous porous medium affected by capillary pressure. Patel Kajal *et al.* <sup>[10]</sup> studied Homotopy analysis method for saturation of injected water in inclination or without inclination during instability phenomena occurred in secondary oil recovery process in inclined porous media. Patel Kaushal *et al.* <sup>[11]</sup> demonstrate the analytical method to analysis saturation of water decrease with an increase in injected fluid and time. Patel *et al.* <sup>[13, 15]</sup> An approximate solution of fingering phenomenon in heterogeneous porous medium with mean pressure explained and fingering phenomena in fluid flow through fracture porous media with inclination and gravitational effect and investigate the applicability of Adomian decomposition method. More Pratiksha *et al.* <sup>[9]</sup> discussed the phenomena in vertical

downward direction in heterogenous porous medium. Meher *et al.* [7] developed the analytical solution of instability phenomenon by Exponential self-similar solution technique with the presence of capillary pressure effect. In previous study, Patel T.R *et al.* [13, 12] have discussed approximate solution water saturation at common interface of instability and fingering phenomena in heterogeneous and homogeneous porous medium with use of power series expansion method. Borana R.N *et al.* [5] also derived solution of instability phenomena in heterogeneous porous medium with help of Crank- Nicolson finite difference method and basic parameters is studied to observe the corresponding effect on saturation of water. Our present effort was focused on use of some different choice of parametric data value and studied the saturation of injected water when water is injected at common interface.

**Mathematical Description**

Certain assumptions were considered when mathematically formulating this phenomenon. The phenomenon of instability in heterogeneous porous media has been studied based on fundamental assumptions: two immiscible fluids, water and oil, flow incompressible; the porous medium is isotropic, incompressible, and finite, with a horizontal and impermeable base; mass conservation holds, and gravitational forces are ignored. The natural oil reservoir is large enough to evaluate the impact of water injection (water flooding) on the oil extraction process. To investigate the instability phenomenon in heterogeneous porous media, we chose a cylindrical segment of porous matrix with length L (Figure. 1), where three surfaces are impermeable except for one end, where water is introduced. The reliability of the water flood depends on the mobility ratio of oil to water, the variability of the porous medium, fluid separation within the reservoir, and the loss of fluid fronts caused by capillary pressure. These frontal instabilities are usually marked by many penetrating extensions of the displacing fluid. As a result, all oil at the starting boundary  $x = 0$  (with  $x$  measured along the direction of movement) is shifted a distance L because of water injection [5].



**Fig 1:** A cylindrical heterogeneous porous matrix is used to illustrate Fingering Phenomenon.

**Mathematical Formulation**

For the double phase flow system, we may express the seepage velocities of the wetting phase and the non-wetting phase by assuming the validity of Darcy’s law [3, 21].

$$V_w = -\frac{k_w}{r_w} K \frac{\partial P_w}{\partial x} \tag{1}$$

$$V_o = -\frac{k_o}{r_o} K \frac{\partial P_o}{\partial x} \tag{2}$$

In this context,  $K$  represents the variable permeability of the fractured porous medium, while  $k_w$  and  $k_o$  denote the relative permeability of the displacing fluid and the native fluid, respectively.  $P_w$  and  $P_o$  represent pressures;  $r_w$  and  $r_o$  denote the constant kinematic viscosities of the displacing and native fluids respectively, the equations of continuity for these two fluids are expressed as,

$$\emptyset \frac{\partial S_w}{\partial t} + \frac{\partial V_w}{\partial x} = 0 \tag{3}$$

$$\emptyset \frac{\partial S_o}{\partial t} + \frac{\partial V_o}{\partial x} = 0 \tag{4}$$

Where,  $\emptyset = \emptyset(x)$  is the porosity of the fractured porous media. The logical direct relationship between capillary pressure and phase saturation can be written as, [19, 20].

$$S_w + S_o = 1 \tag{5}$$

$$P_c = P_o - P_w \quad (6)$$

We consider the capillary pressure and relative permeability function for water as <sup>[6]</sup>,

$$P_c = \beta (S_w^{-\frac{1}{2}} - C_0) \quad (7)$$

Where,  $\beta$  and  $C_0$  are constant of proportionality. Corey's Model, utilized in this paper, provided the standard correlation among relative permeability and phase saturation <sup>[6]</sup>.

$$\begin{aligned} k_w &= S_w^3 \\ k_o &= 1 - \alpha S_w \end{aligned} \quad (8)$$

Where,  $\alpha$  is constant and its value is  $\alpha=1.11$  Since, The porosity and permeability of fractured porous media <sup>[1]</sup>,

$$\phi(x) = \frac{1}{b_1 - b_2 x} \quad (9)$$

$$K(x) = K_c \phi(x) \quad (10)$$

Where,  $b_1 - b_2 x \geq 1$ ; where, a and b are constants, for saturation, Substituting is the key to obtaining the Eq. (1) and Eq. (2) in continuity of the equations respectively, we get,

$$\phi \frac{\partial S_w}{\partial t} = \frac{\partial}{\partial x} \left( \frac{k_w}{r_w} K \frac{\partial P_w}{\partial x} \right) \quad (11)$$

$$\phi \frac{\partial S_o}{\partial t} = \frac{\partial}{\partial x} \left( \frac{k_o}{r_o} K \frac{\partial P_o}{\partial x} \right) \quad (12)$$

Eliminating  $\frac{\partial P_w}{\partial x}$  from Equation (11) and Equation (6), we have

$$\phi \left( \frac{\partial S_w}{\partial t} \right) = \frac{\partial}{\partial x} \left[ \frac{k_w}{r_w} K \left( \frac{\partial P_o}{\partial x} - \frac{\partial P_c}{\partial x} \right) \right] \quad (13)$$

Now From, Eq. (12) and using Eq. (13) we derive,

$$\frac{\partial}{\partial x} \left[ \left( \left[ \frac{k_w}{r_w} + \frac{k_o}{r_o} \right] K \right) \frac{\partial P_o}{\partial x} - \frac{k_w}{r_w} K \frac{\partial P_c}{\partial x} \right] = 0 \quad (14)$$

Integrating Eq. (14) we get,

$$\left[ \frac{k_w}{r_w} K \frac{\partial P_c}{\partial x} - \left( \left[ \frac{k_w}{r_w} + \frac{k_o}{r_o} \right] K \right) \frac{\partial P_o}{\partial x} \right] = V \quad (15)$$

Where, V is the constant of Integration. From Eq. (15)

$$\frac{\partial P_o}{\partial x} = \frac{V}{\left[ \frac{k_w}{r_w} + \frac{k_o}{r_o} \right] K} + \frac{\frac{k_w}{r_w} K}{\left[ \frac{k_w}{r_w} + \frac{k_o}{r_o} \right] K} \frac{\partial P_c}{\partial x} \quad (16)$$

By putting the values of  $\frac{\partial P_o}{\partial x}$  in Eq. (13) it gives,

$$\phi \left( \frac{\partial S_w}{\partial t} \right) + \frac{\partial}{\partial x} \left[ \frac{\frac{k_o}{r_o}}{\left(1 + \frac{k_o r_w}{r_o k_w}\right)} K \frac{\partial P_c}{\partial x} - \frac{V}{\left(1 + \frac{k_o r_w}{r_o k_w}\right)} \right] = 0 \quad (17)$$

The value of the pressure of oil ( $P_o$ ) can be written as,

$$P_o = \bar{P} + \frac{1}{2} P_c \quad (18)$$

Where,  $\bar{P}$  is a constant that signifies the average pressure. Now

$$\left( \frac{\partial P_o}{\partial x} \right) = \frac{1}{2} \left( \frac{\partial P_c}{\partial x} \right) \quad (19)$$

Substituting the value of  $\frac{\partial P_o}{\partial x}$  in Eq. (15) it gives,

$$V = \frac{1}{2} K \left[ \frac{k_w}{r_w} - \frac{k_o}{r_o} \right] \left( \frac{\partial P_c}{\partial x} \right) \quad (20)$$

Substituting the Eq. (19) into Eq. (17), We obtain,

$$\phi \left( \frac{\partial S_w}{\partial t} \right) + \frac{1}{2} \frac{\partial}{\partial x} \left[ \frac{k_w}{r_w} K \frac{dP_c}{dx} \frac{\partial S_w}{\partial x} \right] = 0 \quad (21)$$

Replacing this Value Eq. (7), (8) and Eq. (10) into Eq. (20), We get,

$$\phi \left( \frac{\partial S_w}{\partial t} \right) - \frac{1}{4} \frac{\beta K_c}{r_w} \frac{\partial}{\partial x} \left[ \phi S_w^{\frac{3}{2}} \frac{\partial S_w}{\partial x} \right] = 0 \quad (22)$$

This partial differentiation-based nonlinear equation represents the absorption process of Instability phenomena and demonstrates the equation of motion that saturates the liquid injected into a fractured porous medium.

### Solution of the Problem

Dimensionless Variable is chosen as follow,

$$X = \frac{x}{L} \quad T = \frac{1}{4} \frac{\beta K_c}{L^2 r_w} t \quad (23)$$

Replacing this Value in the Eq. (21), we have,

$$\frac{\partial S_w}{\partial T} - \left( \frac{\partial S_w^{\frac{3}{2}}}{\partial X} \right) \frac{\partial S_w}{\partial X} - \frac{1}{\phi} \frac{\partial \phi}{\partial X} S_w^{\frac{3}{2}} \left( \frac{\partial S_w}{\partial X} \right) - S_w^{\frac{3}{2}} \left( \frac{\partial^2 S_w}{\partial X^2} \right) = 0 \quad (24)$$

Eq. (23) This is a non-linear partial differential equation. For the purpose of simplifying the problem, we will focus on the term  $\frac{1}{\phi} \frac{\partial \phi}{\partial X}$  has been simplified as,

$$\frac{1}{\phi} \frac{\partial \phi}{\partial X} = \frac{\partial}{\partial X} (\log \phi) = L \left( \frac{b_2}{b_1} \right) = \frac{L}{2\sqrt{T}} \text{ (neglacting the higher term of } X) \quad (25)$$

Where,  $\frac{b_2}{b_1} = \frac{1}{2\sqrt{T}}$  for any  $0 < T \leq 1$  Hence, Eq. (23) will be,

$$\frac{\partial S_w}{\partial T} - \left( \frac{\partial S_w^{\frac{3}{2}}}{\partial X} \right) \frac{\partial S_w}{\partial X} - \left( \frac{L}{2\sqrt{T}} \right) S_w^{\frac{3}{2}} \left( \frac{\partial S_w}{\partial X} \right) - S_w^{\frac{3}{2}} \left( \frac{\partial^2 S_w}{\partial X^2} \right) = 0 \tag{26}$$

The Appropriate Boundary Condition to Solve Eq. (25) as,

$$S_{wo}(X, 0) = 0 = S_{wc}, \text{ for } X > 0 \tag{27}$$

$$S_{wo}(0, T) = 1 = S_{wo}, \text{ for } T > 0 \tag{28}$$

$$S_{wo}(1, T) = 0 = S_{wi}, \text{ for } T > 0 \tag{29}$$

Choose the Similarity Transformation <sup>[16]</sup>,

$$S_{wo}(X, T) = f(\zeta) \quad \text{where, } \zeta = \frac{X}{2\sqrt{T}} \tag{30}$$

The governing equation (25) simplifies to a standard ordinary discrimination equation, accompanied by the boundary conditions (26) and (28) that we retain,

$$f(\zeta)^{\frac{3}{2}} f''(\zeta) + \frac{3}{2} f(\zeta)^{\frac{1}{2}} f'^2(\zeta) + L f(\zeta)^{\frac{3}{2}} f'(\zeta) - \zeta f'(\zeta) = 0 \tag{31}$$

With the Boundary Conditions Eq. (26) and Eq. (27),

$$f(0) = S_{wo}, \quad X = 0, T > 0 \tag{32}$$

$$f(\infty) = S_{wc}, \quad T = 0, X > 0 \tag{33}$$

$$f'(0) = \vartheta, \text{ for any } T > 0 \tag{34}$$

To determine the successive coefficients of the Maclaurin series at  $\zeta=0$ . By computing the nth derivative of Equation (30), and then solving for  $f^{m+2}(\zeta)$  and evaluating at  $\zeta=0$ , we have,

$$\begin{aligned} &\sum_{m=0}^n \binom{n}{m} \left( \frac{d^m}{d\zeta^m} f(\zeta)^{\frac{3}{2}} \right) f^{(n-m+2)}(\zeta) = \\ &-\frac{3}{2} \sum_{m=0}^n \binom{n}{m} \left( \frac{d^m}{d\zeta^m} f(\zeta)^{\frac{1}{2}} \right) \left( \frac{d^{n-m}}{d\zeta^{n-m}} (f'(\zeta))^2 \right) \\ &-L \sum_{m=0}^n \binom{n}{m} \left( \frac{d^m}{d\zeta^m} f(\zeta)^{\frac{3}{2}} \right) f^{(n-m+1)}(\zeta) \\ &-n f^{(n)}(\zeta) - \zeta f^{(n+1)}(\zeta) \end{aligned} \tag{35}$$

To solve this, we must get the derivatives of  $f^n(0)$  for all  $n = 1, 2, 3, \dots$ ,  $f'(0)$  can be obtained from Eq. (32) and formula Eq. (30) can be used to find the derivative  $f''(0)$ . By entering  $n = 1, 2, 3, \dots$ , all additional higher derivatives can also be found using formula (34). Consequently, the intended worth of  $f(\zeta)$  can be calculated using Maclaurin's series,

$$f(\zeta) = \sum_{j=0}^{\infty} f^j(0) \frac{\zeta^j}{j!} \tag{36}$$

Therefore, we have,

$$f(\zeta) = f(0) + \zeta f'(0) + \frac{\zeta^2}{2!} f''(0) + \frac{\zeta^3}{3!} f'''(0) + \frac{\zeta^4}{4!} f^{iv}(0) + \dots \tag{37}$$

$$S_w(X,T) = f(0) + \frac{X}{2\sqrt{T}} f'(0) + \frac{X^2}{8(\sqrt{T})^2} f''(0) + \frac{X^3}{48(\sqrt{T})^3} f'''(0) + \frac{X^4}{384(\sqrt{T})^4} f^{iv}(0) + \frac{X^5}{3840(\sqrt{T})^5} f^v(0) + \dots \tag{38}$$

Now From Eq. (28),

Where,

$$f(0) = S_{wo}$$

$$f'(0) = \vartheta$$

$$f''(0) = -3 \left[ \frac{\vartheta^2}{S_{wo}} + L\vartheta \right]$$

$$f'''(0) = - \left[ \frac{3 \vartheta^3}{4 S_{wo}^2} + \frac{9 \vartheta f''}{2 S_{wo}} + \frac{3L \vartheta^2}{2 S_{wo}} + \frac{\vartheta}{S_{wo}^{\frac{3}{2}}} + Lf'' \right]$$

$$f^{iv}(0) = - \left[ 6 \frac{\vartheta f^{iv}}{S_{wo}} - \frac{3 \vartheta^4}{8 S_{wo}^3} + \frac{9 f'' \vartheta^2}{2 S_{wo}^2} + \frac{9 f''^2}{2 S_{wo}} + \frac{9 L \vartheta f''}{2 S_{wo}} + \frac{3L \vartheta^3}{4 S_{wo}^2} + \frac{2f''}{S_{wo}^{\frac{3}{2}}} + Lf''' \right]$$

$$f^v(0) = - \left[ \frac{15 \vartheta f^{iv}}{2 S_{wo}} + \frac{6L \vartheta f'''}{S_{wo}} + \frac{15 f'' f'''}{S_{wo}} + \frac{9L f''^2}{2 S_{wo}} + \frac{15 \vartheta^2 f'''}{2 S_{wo}^2} + \left( \frac{9L}{2} + 9 \right) \frac{\vartheta^2 f''}{S_{wo}^2} + \frac{9 \vartheta f''^2}{4 S_{wo}^2} - \frac{15 \vartheta^3 f''}{4 S_{wo}^3} - \frac{3L \vartheta^4}{8 S_{wo}^3} + \frac{9 \vartheta^5}{16 S_{wo}^4} + \frac{3f'''}{f^{\frac{3}{2}}} \right] \tag{39}$$

The equation is when water is added to the general interface processes for recovering secondary oil, such as, in fractured porous environments, Eq. (36) demonstrates that liquid injection saturation takes place during the Fingering phenomena.

**Analysis of Convergence**

The Convergence of the Maclaurin Series Eq. (36) depends on the growth of the co-efficient  $f^j(0)$ . From the recurrence relation Eq. (34), Each higher derivatives is expressed as a finite combination of lower order derivatives and polynomial non linearities in  $f$ . Assume there exists Constant C,  $M > 0$  Such that,

$$|f^j(0)| \leq CM^j j! \text{ for all } j \geq 0. \tag{40}$$

Then the general term,

$$u_j = \frac{f^j(0)}{j!} \zeta^j \text{ satisfies } |u_j| \leq C(M|\zeta|)^j \tag{41}$$

Now, Apply Cauchy Root Test for convergence,

$$\lim_{j \rightarrow \infty} \sup |u_j|^{\frac{1}{j}} \leq M|\zeta| \tag{42}$$

Therefore, the series converges for  $|\zeta| < \frac{1}{M}$ . Therefore, The Maclaurin series has a finite ROC given by  $R = \frac{1}{M}$  series is locally convergent but not globally.

Saturation  $S_w(X, T)$  vs. Distance  $X$

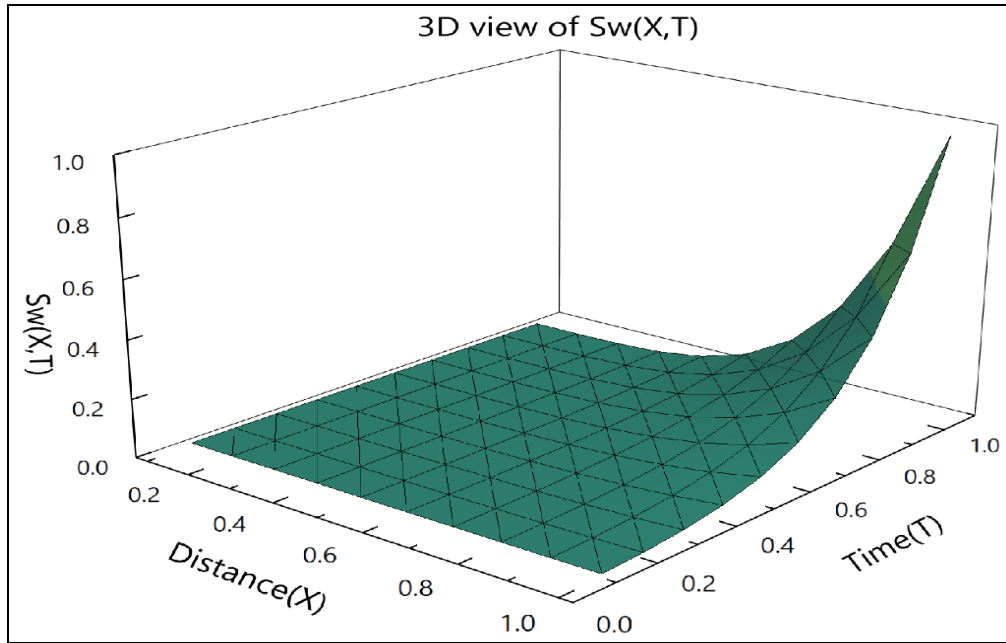


Fig 2:  $S_w(X, T)$  when  $T=0.1$  to  $1$  and  $\theta=0.01$ ,  $S_{wo}=0.0162$ ,  $L=5$

Table 1: Numerical assessment of the Fingering Phenomenon in Fractured Porous Media.

X	T	T	T	T	T	T	T	T	T	T
	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9	1
0.1	0.0162	0.0162	0.0163	0.0163	0.0163	0.0163	0.0163	0.0163	0.0163	0.0164
0.2	0.0162	0.0162	0.0163	0.0163	0.0163	0.0164	0.0164	0.0165	0.0166	0.0167
0.3	0.0162	0.0163	0.0164	0.0165	0.0166	0.0169	0.0172	0.0176	0.0182	0.0190
0.4	0.0162	0.0164	0.0167	0.0171	0.0176	0.0185	0.0197	0.0214	0.0240	0.0276
0.5	0.0163	0.0167	0.0174	0.0185	0.0201	0.0224	0.0260	0.0313	0.0391	0.0504
0.6	0.0164	0.0172	0.0188	0.0212	0.0249	0.0305	0.0390	0.0519	0.0711	0.0991
0.7	0.0166	0.0183	0.0213	0.0261	0.0335	0.0450	0.0628	0.0901	0.1311	0.1913
0.8	0.0170	0.0199	0.0253	0.0339	0.0474	0.0688	0.1025	0.1547	0.2337	0.3501
0.9	0.0175	0.0224	0.0312	0.0456	0.0687	0.1058	0.1650	0.2573	0.3979	0.6059
1	0.0183	0.0259	0.0397	0.0626	0.0998	0.1605	0.2582	0.4121	0.6475	0.9972

Quantitative Results and Analysis

During the secondary oil recovery process, when water is injected, the solution Eq. (37) illustrates the saturation of the injected fluid, which is an ascending power series of  $X$  with time  $T > 0$ . The answer Eq. (36) which is also in terms of power series in  $\zeta$ , satisfies constraints Eq. (31) and (32) as well. As we have just examined the first five terms in the power series, it provides a rough explanation for the instability phenomenon and also shows that the convergent power series. We saw water saturation from the graph at  $X=0$  when the instability phenomena happen at the common interface for a certain value of the parameter.

Figure 2 depicts the graph of  $S_w(X, T)$  vs distance measured from the common interface in dimensionless variables. At time  $T=0.1$ , the saturation graph continuously increases until  $X=1$ , where it abruptly increases due to the initial unsaturation of the fractured porous medium. For various values of  $X$ , the saturation of water increases consistently while time  $T$  grows to  $T=0.1-1$ ; The Numerical Solution for the governing Eq. (25) representing instability phenomenon in fractured porous media is

obtained by using Maclaurin's series given by the Eq. (36) and (37). The term  $\frac{L}{2\sqrt{T}}$  that appears in Eq. (25) is referred to as the heterogeneity coefficient for the governing equation, if  $\frac{L}{2\sqrt{T}} = 0$ . It describes the phenomenon of instability in a homogeneous porous medium. The numerical values representing the saturation of water at different time intervals are displayed in Table 1, In conjunction with its graphical depiction from Figure 2, It is evident that the saturation of water rises over time and also increases with distance  $X$ . Therefore, the physical reality of the issue is maintained in the scenario of a fractured porous medium, allowing for a significant quantity of oil to be displaced.

Conclusion

The investigation shows water saturation increases uniformly with distance and time, indicating a stable displacement front with negligible viscous fingering. Viscous and capillary forces suppress instabilities, ensuring a smooth saturation profile.

Early-stage, localized fingering in fractures due to permeability and velocity variations diminishes over time without affecting overall stability. Power-series representation confirms gradual saturation rise from  $S_{w0}=0.0162$ , with minimal interface disturbance. The analytical solution captures initial fingering at  $X=0$ , while numerical results show consistent saturation increase with radial distance and time. Permeability, capillary pressure, and injection rate variations in fractured media strongly influence saturation and displacement dynamics. The model improves predictive accuracy, enhances sweep efficiency understanding, and demonstrates stable, uniform flow (Table 1, Figure 2).

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### Conflict of Interest

The Authors declared that they have no conflict of interest.

### Nomenclature

$V_w$	Velocity of water in the wetting phase [m/s]
$V_o$	Velocity of the oil in the non-wetting phase [m/s]
$K$	Porous medium's permeability [ $m^2$ ]
$k_w$	Permeability to the wetting phase [ $m^2$ ]
$k_o$	Permeability to the non-wetting phase [ $m^2$ ]
$P_w$	Pressure of the water in the wetting phase [Pa]
$P_o$	Pressure of the oil in the non-wetting phase [Pa]
$\phi$	The porous medium's porosity (volume of voids/total volume)
$S_w$	Saturation of the wetting phase (water) (volume of water / volume of voids)
L	characteristic length [m]
T	Dimensionless time [Sec]
$r_o$	oil viscosity
$r_w$	Water viscosity
$P_c$	capillary pressure
$\beta$	Proportionality Constant

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